$$N_T = N_0 \cdot 2^{(T/g)}$$

as time increases, $t/g = 1, 2, 3$ ..., thus 2^1, 2^2, 2^3, etc.

g is the generation time

N_0 is the number of cells at time T = 0

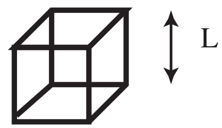
N_T is the number of cells at time T

Logistic growth curve:

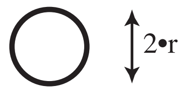
$$N_T = \frac{K \cdot N_0 \cdot e^{T/g}}{K + N_0(e^{T/g} - 1)}$$

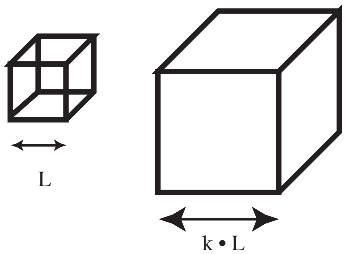
K is the carrying capacity

A cube has a surface area of $6 \cdot L^2$. Its volume is L^3. As long as the shape is constant, the ratio of suraface area to volume will always be $(6 \cdot L^2) / L^3$, or $6/L$.



For a sphere, the surface area is $4 \cdot \pi \cdot r^2$, and the volume is $\pi \cdot r^3$; the corresponding ratio of surface area to volume is $4/r$.





(area) $A_1 = 6 \cdot L^2$ $\quad A_k = 6 \cdot (k \cdot L)^2 \quad A_k = 6 \cdot k^2 \cdot L^2 \quad (= k^2 \cdot A_1)$

(volume) $V_1 = L^3$ $\quad V_k = (k \cdot L)^3 \quad V_k = k^3 \cdot L^3 \quad (= k^3 \cdot V_1)$

The scaling coefficient is different for area (k^2) and for volume (k^3).

Heat conduction rates are defined by the relation:

$$P_{cond} = Q / t = k \cdot A \cdot [(T_a - T_b) / L]$$

where P_{cond} is the rate of conduction (transferred heat, Q, divided by time, t); k is the thermal conductivity; T_a and T_b are the temperatures of the two heat reservoirs a and b; A is the area; and L is the distance. Thermal conductivities of water and air are about 0.6 and 0024 W m^{-1} K^{-1}, respectively.

Thermal radiation is defined by the relation:

$$P_{rad} = \sigma \cdot \varepsilon \cdot A \cdot T^4$$

where P_{rad} is the rate of radiation; σ is the Stefan-Boltzmann constant ($5.6703 \cdot 10^{-8}$ W m^{-2} K^{-4}; ε is the emissivity (varies from 0 to 1, where 1 is for a blackbody radiator); A is the area; and T is the temperature (in Kelvins). The *net* radiative emission or absorption will depend upon the difference in temperature:

$$P_{net} = \sigma \cdot \varepsilon \cdot A \cdot (T^4_{body} - T^4_{ambient})$$

$$\text{compression} = \rho \cdot h$$

$$h_{critical} = \frac{42.4 \cdot 10^6 (\mathrm{N} \cdot \mathrm{m}^{-2}) \cdot \frac{1(\mathrm{kg(f)})}{9.80665(\mathrm{N})}}{436(\mathrm{kg} \cdot \mathrm{m}^3)}$$

$$F_{cr} = \frac{E \cdot I \cdot \pi^2}{L^2_{eff}}$$

$$F_{cr} = \frac{E \cdot \frac{\pi \cdot r}{4} \cdot \pi^2}{(2 \cdot h)^2}, \text{ and } F_{cr} = \rho \cdot \pi \cdot r^2 \cdot h$$

$$\Psi_{wv} = \frac{RT}{\bar{V}_w} \ln\left(\frac{\%\text{ relative humidity}}{100}\right) + \rho_w g h$$

velocity (meters sec^{-1})

pressure difference (Pascal = 1 kg m^{-1} sec^{-1})

tube radius

$$v = \left(\frac{\Delta p}{l}\right)\left(\frac{1}{4 \cdot \eta}\right)(R^2 - r^2)$$

distance (meters)

viscosity (water = 0.01 gm cm^{-1} sec^{-1}, or Pa sec)

distance from center of tube

$$v = \left(\frac{\Delta p}{l}\right)\left(\frac{1}{4 \cdot \eta}\right) R^2 \qquad J_v = \left(\frac{\Delta p}{1}\right)\left(\frac{\pi}{8 \cdot \eta}\right) \cdot R^4$$

density (water = 1 gm cm^{-3})

velocity (cm sec^{-1})

tube diameter (cm)

$$R_e = \frac{\rho \cdot v \cdot l}{\eta}$$

viscosity (water = 0.01 gm cm^{-1} sec^{-1})

$$J = -D\frac{\partial c}{\partial x}$$

Fick's First Law of Diffusion: The flux is proportional to the concentration gradient

$$\frac{\partial c}{\partial t} = -\frac{\partial J}{\partial x}$$

Fick's Second Law of Diffusion: Changes in concentration over time depend upon the flux gradient

$$\frac{\partial c}{\partial t} = D\frac{\partial^2 c}{\partial x^2}$$

$$J = -\frac{1}{2} \bullet \frac{\Delta^2}{\tau} \bullet \frac{dC}{dx}$$

$$D = \frac{1}{2} \bullet \frac{\Delta^2}{\tau}$$

$$\nabla \nu = u\frac{\partial}{\partial x} + v\frac{\partial}{\partial y} + w\frac{\partial}{\partial z}$$

velocity vector
—the notation grad ν
is sometimes used

with velocity components, u, v, and w,
in the three dimensions, x, y, and z.

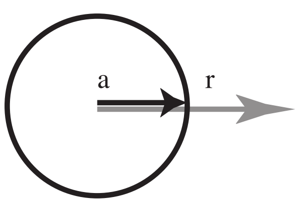
$$J_x = -D\frac{\partial c}{\partial x} + v_x \bullet c$$

units: moles cm^{-2} sec^{-1}

(cm^2 sec^{-1})(moles cm^{-4})

(cm sec^{-1})(moles cm^{-3})

$$J_V = -\frac{r^2}{8 \bullet \eta} \bullet \frac{\partial P}{\partial x}$$



Fick's First law : $J_r = -D\frac{\partial C}{\partial r}$

Fick's Second Law :
(steady state)

$$C(r) = C_0\left(1 - \frac{a}{r}\right)$$

$$\frac{\partial C}{\partial t} = D\frac{1}{r^2}\frac{\partial}{\partial r}\left(r^2\frac{\partial C}{\partial r}\right) = 0$$

$$J_r(a) = -D \bullet C_0 \bullet 4 \bullet \pi \bullet a = I_D \text{ (diffusive current)}$$

(units of mole sec^{-1})

(mole cm^{-2} sec^{-1})

$$I_m = 4 \bullet \pi \bullet a^2 \bullet \beta \text{ (metabolic current)}$$

(cm^2) (units of mole sec^{-1})

$$\frac{\partial C}{\partial t} = u \bullet \frac{\partial C}{\partial r} \bullet C + D\frac{\partial^2 C}{\partial r^2}$$

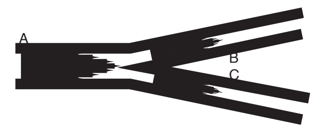
flow velocity

concentration gradient

concentration

$$P_e = \frac{2 \bullet a \bullet u}{D}$$

$$Q = \frac{\Delta p}{l}\frac{\pi a^4}{8\eta}$$



$$\mu_j^{liquid} = \mu_j^* + RT\ln a_j + \overline{V}_j P + z_j FE + m_j gh$$

fluid density

velocity

$$D = \frac{1}{2} \bullet \rho \bullet V^2 \bullet A \bullet C_D$$

frontal area

drag coefficient
(shape-dependent)

$$m\left(-\frac{d\upsilon}{dt}\right) = 6 \bullet \pi \bullet \eta \bullet r \bullet \upsilon$$

$$\upsilon(t) = \upsilon_0 e^{\left(-\frac{6 \bullet \pi \bullet \eta \bullet r}{m} \bullet t\right)}$$

$$p_o(t) = e^{-\lambda}$$

$$p_n = e^{-\lambda T}\frac{(\lambda T)^n}{n!} = \frac{e^{-\mu}\mu^k}{k!}$$

$$\text{Rotor}_{(n)} + mH^+_{\text{outside}} \longleftrightarrow \text{Rotor}_{(n+1)} + mH^+_{\text{inside}}$$

$$\text{ADP} + \text{P}_i + \text{mH}^+_{\text{outside}} \longleftrightarrow \text{ATP} + \text{mH}^+_{\text{inside}}$$

gas constant

Faraday constant

Voltage

$$\mu = \mu^{\circ} + \text{RT}\ln(a_{H^+}) + zF\Psi$$

temperature

activity of protons

$$\Delta \text{G}_{\text{ATP}} = \Delta \text{G}^{\circ}_{\text{ATP}} + \text{RT}\ln\left(\frac{[ATP]}{[ADP][P_i]}\right)$$

$$\Delta \text{G}_{\text{total}} = n \bullet \Delta\mu_{H^+} + \Delta G_{ATP} = 0$$

$$n \bullet \left(RT\ln\left(\frac{a_{H^+}^{inside}}{a_{H^+}^{outside}}\right) + F\Delta\Psi\right) + \Delta G^{o}_{ATP} + RT\ln\left(\frac{[ATP]}{[ADP][P_i]}\right) = 0$$

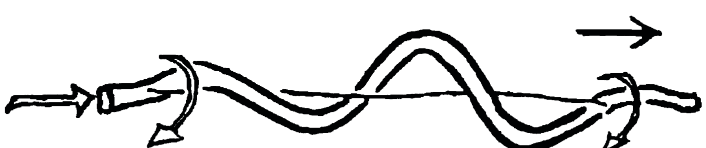
$$\Delta\mu_{H^+} = \frac{RT}{F}\ln\left(\frac{a_{H^+}^{inside}}{a_{H^+}^{outside}}\right) + \Delta\Psi \quad \text{(units: mV)}$$

RT/F is about 25 mV at 20ºC.

$$F = A\upsilon + B\omega$$

$$N = C\upsilon + D\omega$$

That is, both velocity and rotation contribute to both the force and torque.



The work exerted will depend upon the speed of the contraction, and the cross-sectional area of the muscle times its length. Muscle contraction speeds are normally in the range of 3 milliseconds. The initial velocity will equal the impulse force divided by the mass ($\nu = F_{\text{impulse}}$/mass).

The work done in the leap is proportional to mass and the height of the leap ($W \propto mH$), while the work of the muscles is proportional to the mass of the muscle (or the whole organism) ($W \propto m$). It follows then, that the total work is related solely to the height, since the organism's mass cancels out. Thus, the height of the leap is not proportional to the organisms's size, but rather is similar for any organism. D'Arcy Thompson describes this as an example of the Principle of Biological Similitude.

$$\mu_j^{liquid} = \mu_j^* + RT\ln a_j + \overline{V_j}P + z_jFE + m_jgh$$

$$RT\ln a_j + \overline{V_j}P + m_jgh$$

gravitational potential

$$a_j = \gamma_j c_j$$

The activity of water (a_j) is the product of the activity coefficient and the concentration of water

$$\overline{V_j} = \left(\frac{\partial V}{\partial n_j}\right)_{n_i, T, P, E, h}$$

The partial molal volume of species j is the incremental increase in volume with the addition of species j. For water, it is 18.0 X 10^{-6} m^3 mol^{-1}.

$$RT\ln a_j = \overline{V_j}\Pi$$

osmotic pressure

$$\Pi_s = RT\sum_j c_j$$

Van't Hoff relation

The terms inter-relate various properties of water: changes in its activity with the addition of solutes, and the relation to pressure.